



WOC3 Study Group 3.2

WGC 2009



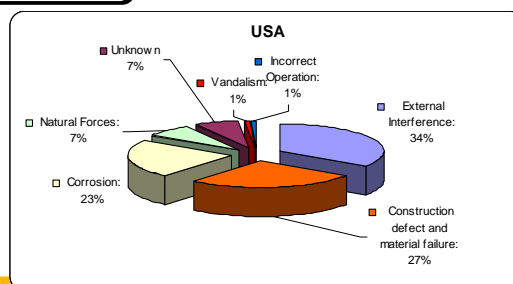
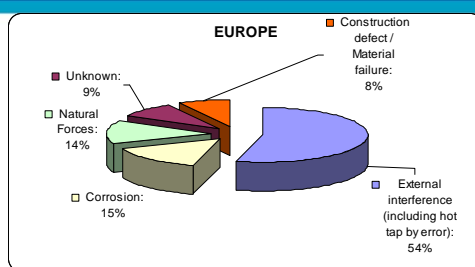
The objective of the SG3.2 is to develop a consensus on the technical needs and challenge for future R&D and to support the exchange of information among the experts of the gas industry.

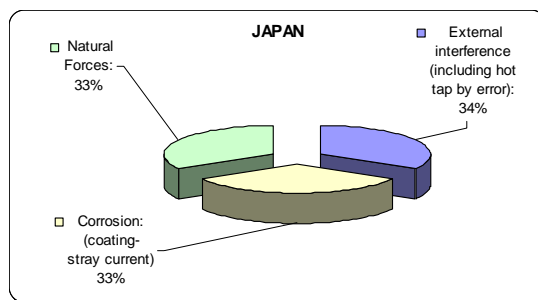
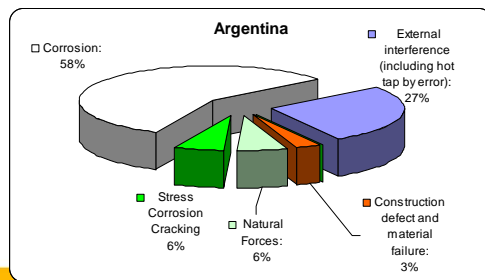
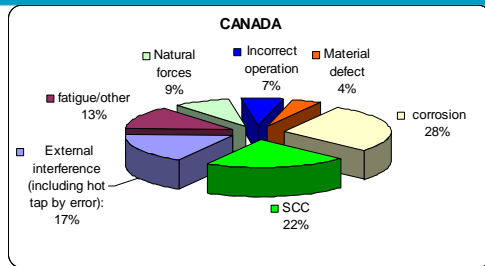
- a) Identification of the general problems affecting the gas transmission industry in the different geographical areas
- b) Evaluation of new tools and methodologies available in the Gas Transmission industry to manage existing problems related with a).
- c) Developing contributions by the SG 3.2 on specific issues, through the support of the Members of the SG related with a)



a) Identification of the general problems affecting the gas transmission industry in the different geographical areas

- The information was submitted by the members of the Study group, trying to cover the different geographical areas in accordance with their respective countries.
- The main common threats of the Gas Industry have been identified and listed for its evaluation
- Europe – USA – Canada – Japan- South America (Argentina)







Europe :

- 1st) External interference " third party damages" (54%)
- 2nd) Corrosion (15%)
- 3rd) Natural Forces (Ground movements) (14%)

USA :

- 1st) External interference " third party damages" (34%)
- 2nd) Materials and construction defects (27%)
- 3rd) Corrosion (23%)

Canada :

- 1st) Corrosion (including SCC) (50%)
- 2nd) External interference " third party damages" (17%)
- 3rd) Fatigue / others (13%)

Argentina:

- 1st) Corrosion(including SCC) (64%)
- 2nd) External interference " third party damages" (27%)
- 3rd) Ground movements & SCC (6%)



The most common and relevant threats in the studied geographical regions are:



•Third party damages



•Corrosion

As a preliminary conclusion, those threats should be taken into account with high priority for the developments on new technologies, because of the risk level involved.



b) Evaluation of new tools and methodologies available in the Gas Transmission industry to manage existing problems

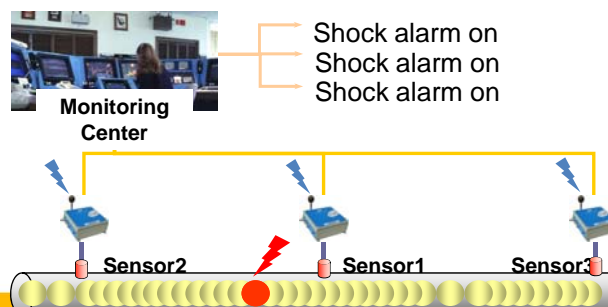
- The information was supplied by the members, and three of them have been evaluated.



1) Third party damages – Early warning !!!

As the Third party damages is not a problem generated by the pipeline itself, but not because of the action of third parties,,there is no way to avoid it 100%,, and the only possibility we found was to be warned as soon as possible in order to minimize its consequences

Shock Detection Process Overview



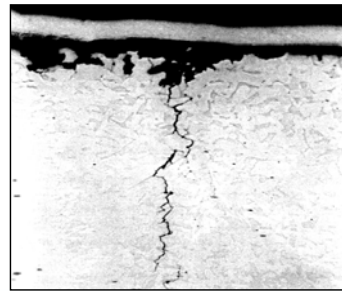


2) Susceptibility model for finding sites with high pH SCC

1) Hydrostatic test : Very expensive and not always possible to execute.

2) ILI : There is not a satisfactory available tool for finding high pH SCC in gas pipelines yet

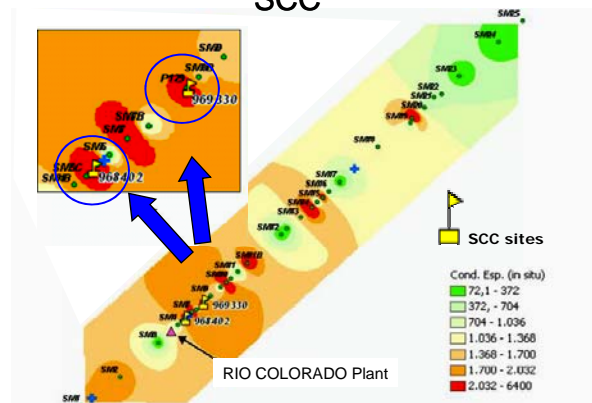
- **Liquid – coupled UT** too cumbersome and expensive
- **MFL + TFI** has not adequate discrimination
- **EMAT** 's possibilities still need to be demonstrated in field operation



(Magnified 250 times)



2) Susceptibility model for finding sites with high pH SCC



So far, modeling is the most cost effective method.



3) Volumetric scanner for metal loss evaluation

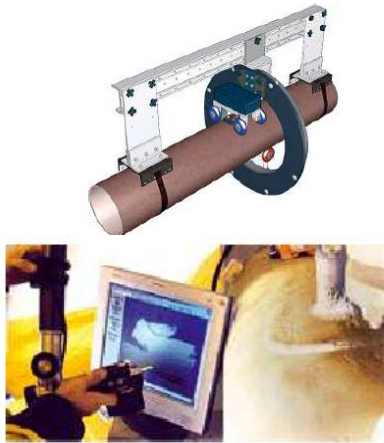


Figura 4.

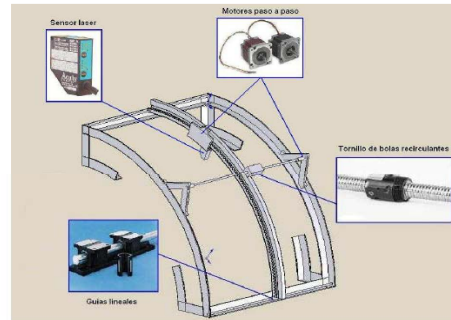
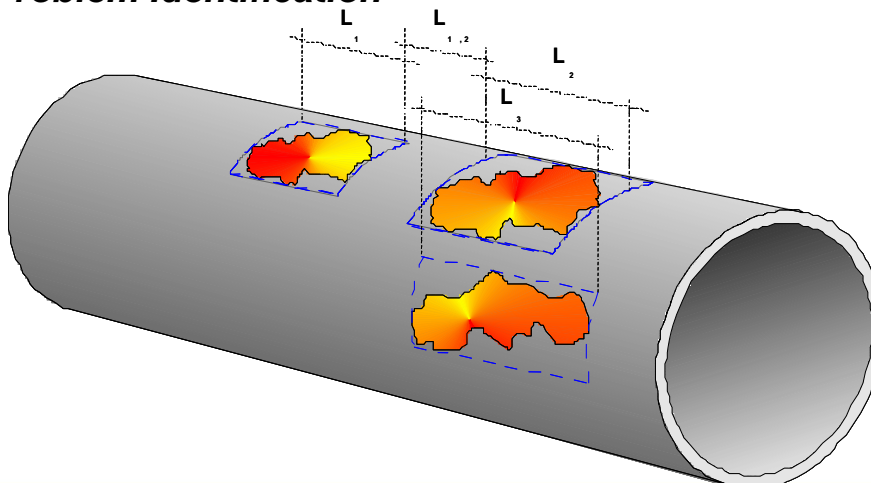


Figura 7. Bastidor curvo con barrido tangencial.

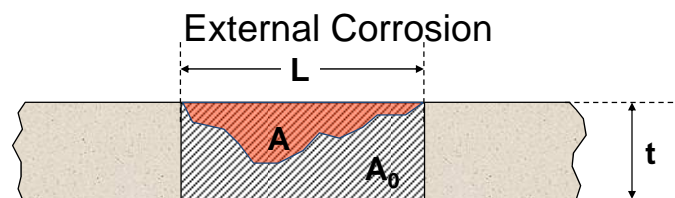


Problem Identification





Failure Stress Determination



$$S_f = S \times \left[\frac{1 - \frac{A}{A_0}}{1 - \frac{A}{A_0} M^{-1}} \right]$$

- S_f = Failure Stress
- S = Yield Stress
- A = Metal loss area
- A_0 = Original area
- M = Folias factor $f(L, D, t)$
- t = Wall thickness
- L = Defect length

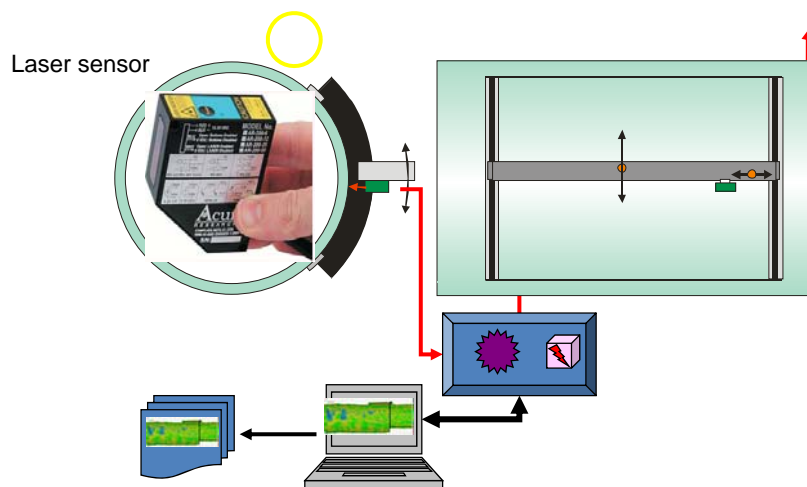


“Traditional” Corrosion Dimension Measurements





“Traditional “ Corrosion Dimension Measurements





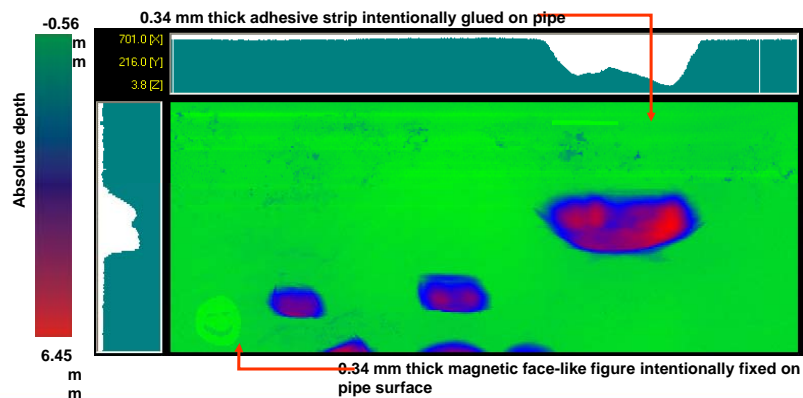
On duty..



Corrosion Measurement

Results on real 30" pipe

Image after automatic surface pipe identification and correction

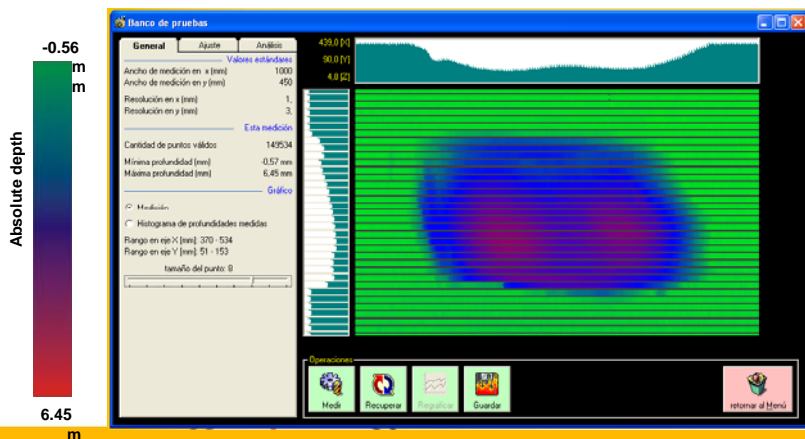




Corrosion Measurement

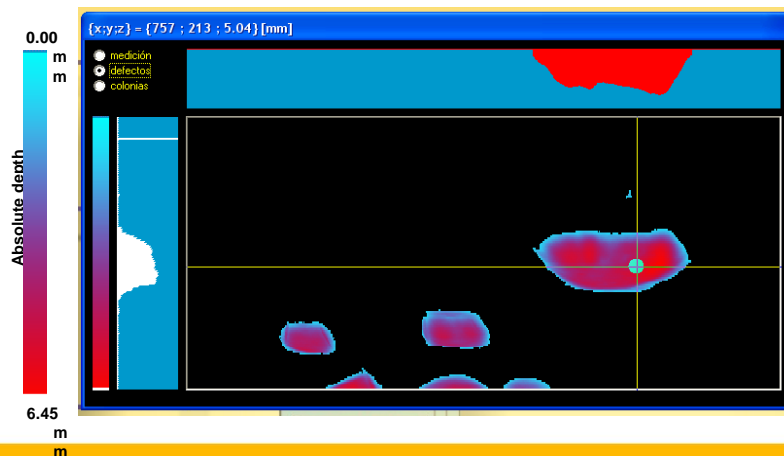
Results on real 30" pipe

Zoom view of a defect



Corrosion Measurement

Automatic Defect Identification According to International Standards





Corrosion Measurement

Automatic Defect Identification According to International Standards

Analisis de medicion

Datos de la medicion:

Código interno	PLEASE tw	Operador	MEYER, Gabriel
Gasoducto	NEUBA I	Denominación	
Tramo	Santa Rosa	Fecha	21.08.2007
		Falla/pozo	1 de 2

Parámetros de análisis:

Esesor real (mm)	0.5	Profundidad mínima para inclusión en defecto (mm)	0.65
Diámetro nominal (pulg)	30	Regla de interacción axial (mm)	51
SMYS (psi)	30000	Regla de interacción transversal (mm)	51
MAPO (bar)	50		
Factor de diseño	1		

Resultado del análisis:

Cluster	Máx. presión segura (bar)	Presión de rotura (bar)	F	Máx. profundidad (mm)
1	40.2	40.2	0.67	5.6
2	46.1	46.4	0.77	4.9
3	31.9	31.9	0.53	6.5
4	46.1	61.5	1.02	1.7

cluster 1:

Norma	Máxima presión segura (bar)	Presión de rotura (bar)	F - Factor de seguridad
Área efectiva	40.2	40.2	0.67
Área 0.85dL	37.7	37.7	0.63
ASME B31G	35.5	35.5	0.59

Presión calculada (bar): 46.1 máxima profundidad (mm): 5.6
 área efectiva (mm²): 0.0 máxima profundidad / esesor real: 0.65
 longitud total (mm): 175.0 desde (mm): 154.5 - hasta (mm): 329.5
 longitud efectiva (mm): 154.0 desde (mm): 164.5 - hasta (mm): 318.5



As a conclusion, all the different geographical areas in the world are sharing two main threats and, despite of the fact that some special issue could be more dangerous for a particular region, helping to solve them will give the industry the most effective actions to run pipelines in a safer way.



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for Natural Gas

Thank you very much!!!