

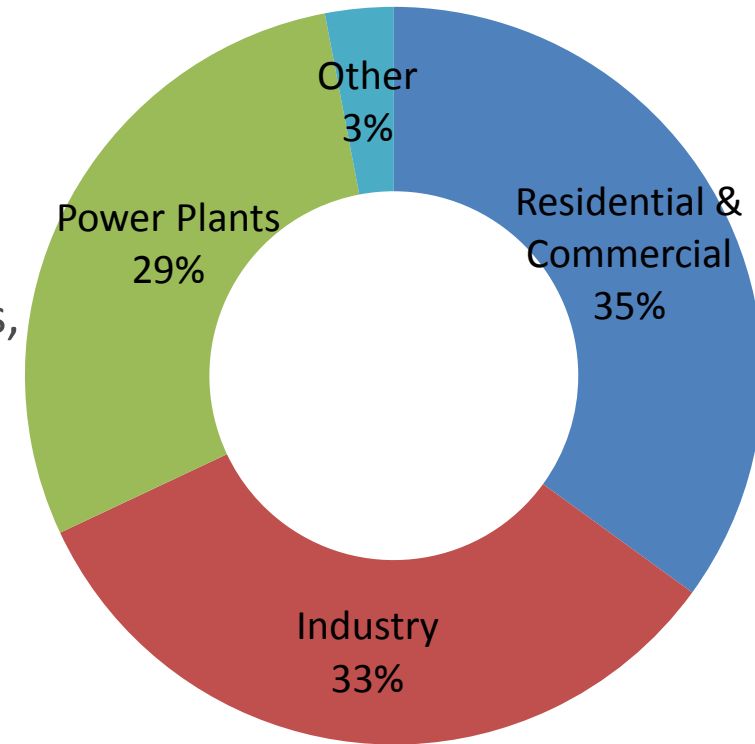


Impact of Changing Natural Gas Quality on Industrial Combustion Processes

IGRC 2014, Copenhagen

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- Industrial applications (excluding power generation) account for about 1/3 of Europe's consumption of natural gas.
- Natural gas is the premier means to provide process heat in many industries, from the food industry to high temperature processes in glass, ceramics and metals manufacturing.
- Manufacturing processes have very high demands for efficiency, stability, pollutant emissions and of course product quality. This usually requires a tight control of furnace conditions.
- Constant natural gas qualities are a significant locational advantage when running sensitive thermal manufacturing processes.

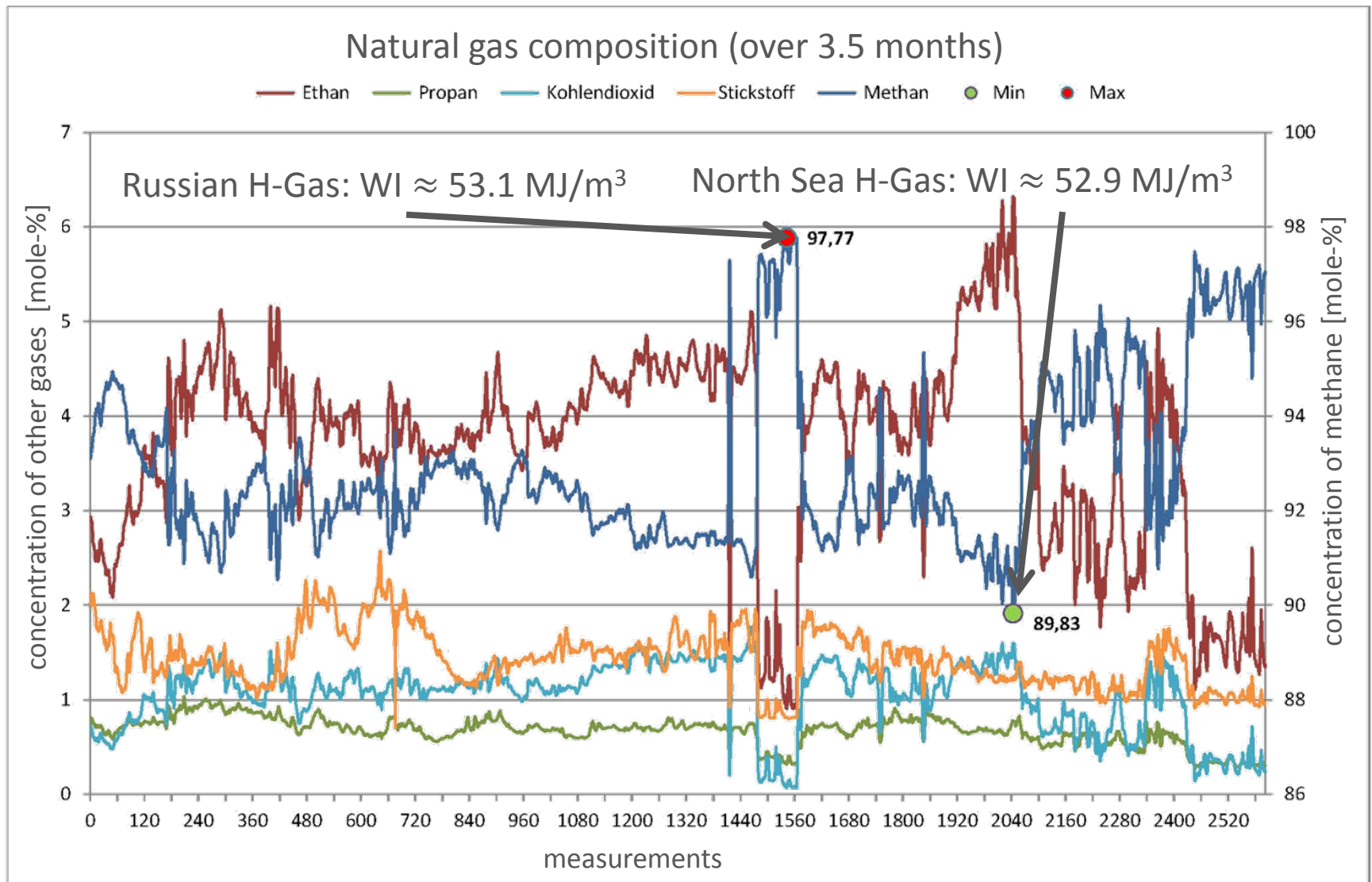


Source: EUROGAS

- The international markets for natural gas are changing for a variety of reasons:
 - Decline of L-Gas from European sources
 - Increasing importance of imports (Russia, Middle East, LNG)
 - New gases: biogas, LNG, possibly H₂ from power-to-gas applications in the near future
 - „Unbundling“, short term supply contracts
 - Harmonization of European gas quality standards (prEN 16726)

- These changes bring a number of benefits to both private and industrial gas consumers, but they also mean that end users will face greater fluctuations in gas quality at any given location within the supply grid.

- For many industrial users, this is a new situation, for which they are often ill-prepared. Some are not even aware of the changing situation.



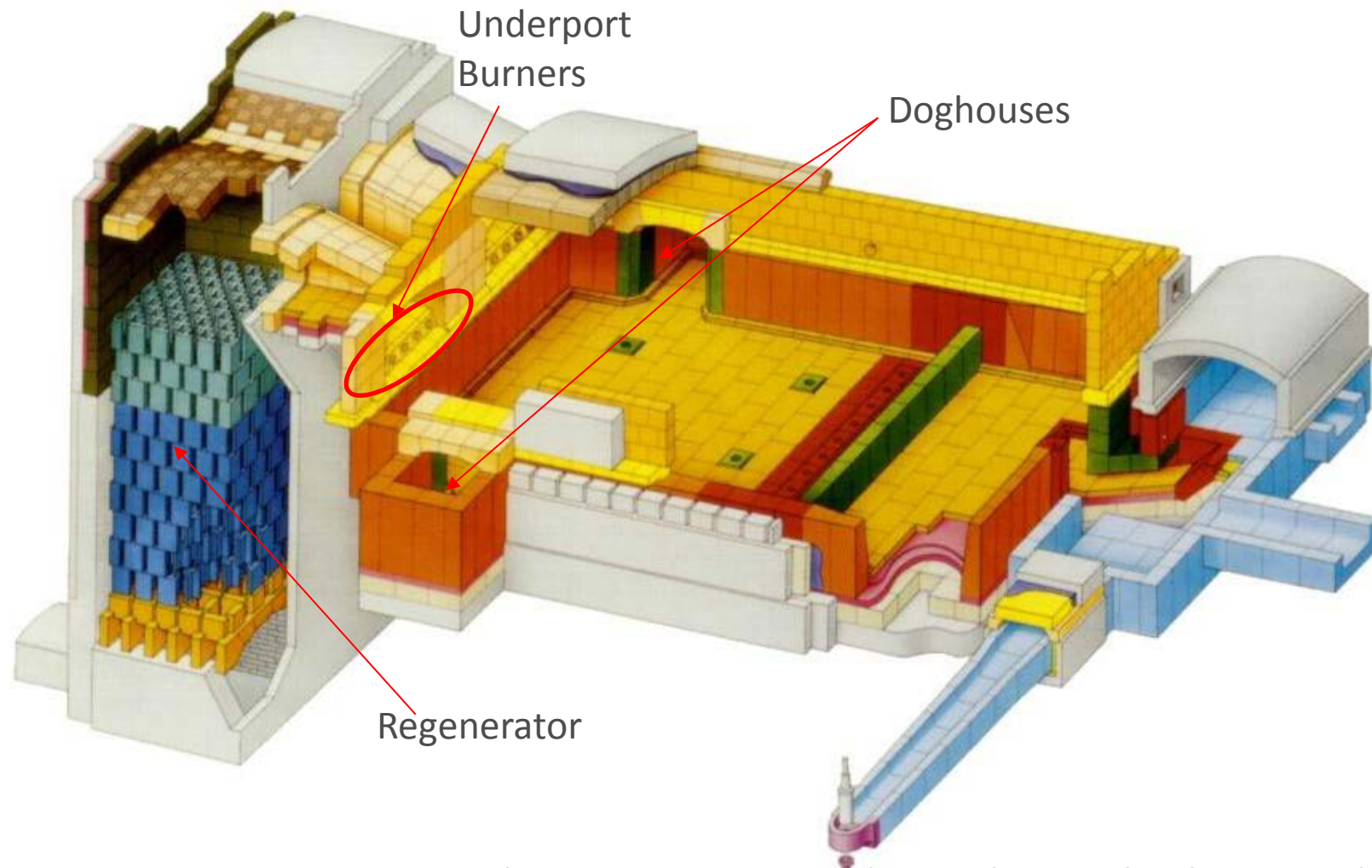
- The potential impacts of changing gas qualities on industrial combustion processes in Germany were investigated in a DVGW-funded research project.
- Both experiments with semi-industrial burner test rigs and CFD analysis were used to examine a number of industrial applications.
- Various scenarios and control strategies were simulated.
- The impacts of gas quality changes on various gas-fired manufacturing processes were assessed.



CFD Case Study: Glass Melting Furnace

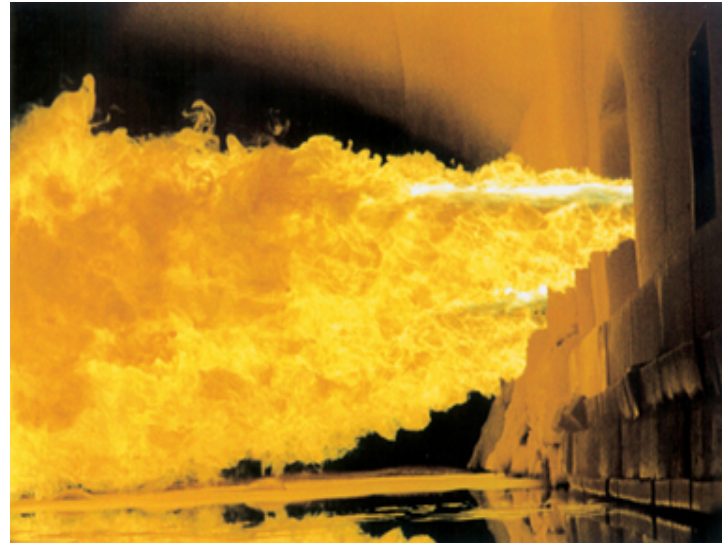
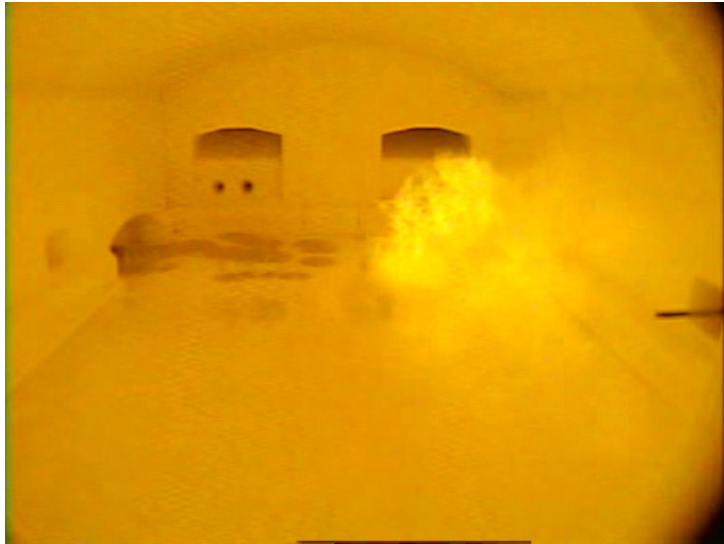


Regenerative Glass Melting Furnace



Source: C. P. Ross; G. L. Tincher; M. Rasmussen: Glass melting technology: a technical and economic assessment, GMIC, 2004

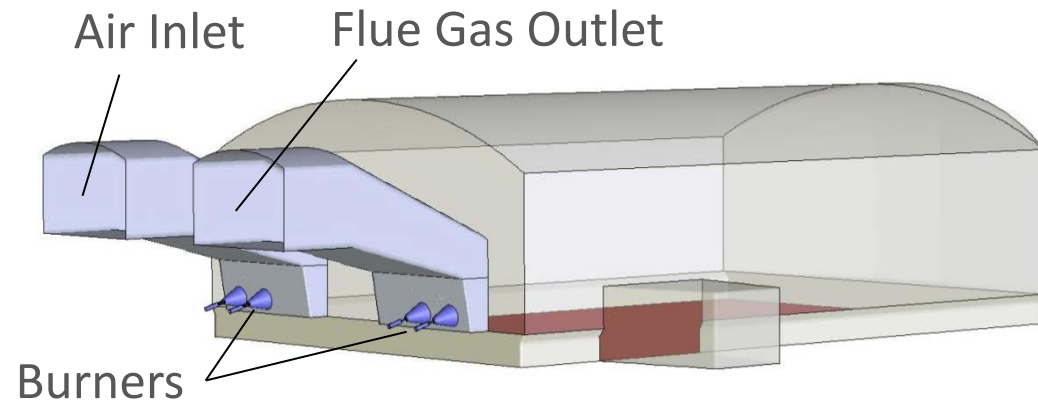
Impressions from the Interior of the Furnace



Source: HVG

Operating Parameters (Reference Case):

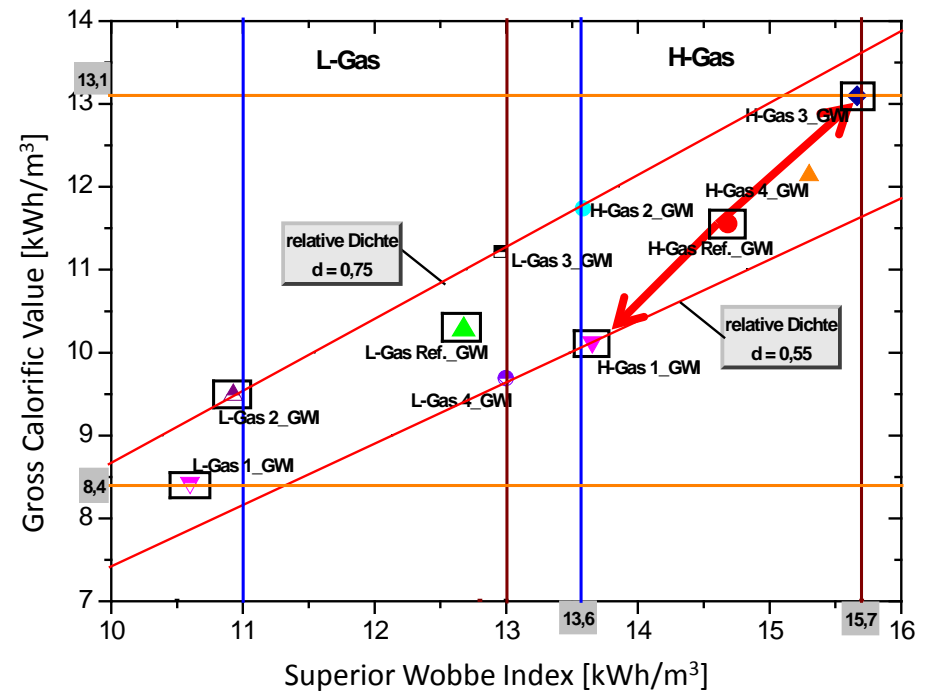
- Load Burner 1: 2000 kW
- Load Burner 2: 2000 kW
- Air Ratio: 1.05
- Gas Temperature: 20 °C
- Air Temperature: 1300 °C
- Glas Melt Surface Temperature: Profile



Approach:

- Test gases at the extremes of German gas quality code DVGW G260 were defined
- Process was adjusted for reference gas and then supplied with another test gas
- Steady CFD simulations were used to examine the impact of a gas quality change
- Various furnace control strategies were investigated

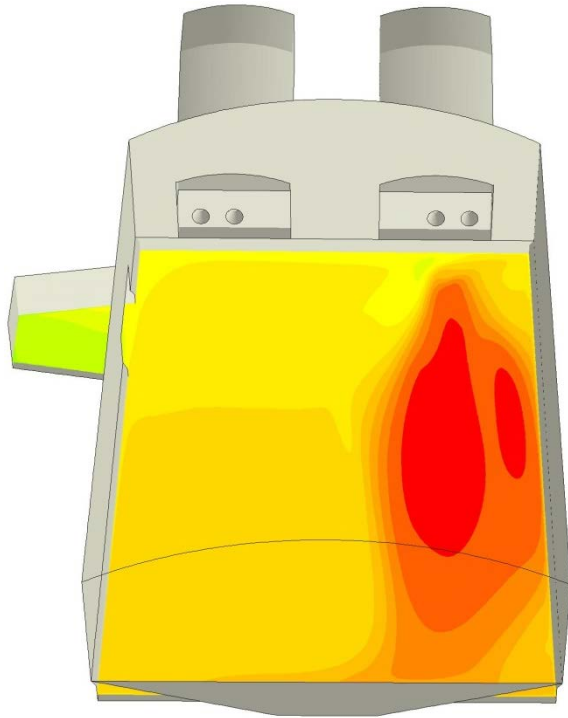
- Fuel gas composition changes from H-Gas Ref._GWI to H-Gas 1_GWI or H-Gas 3_GWI... an oxygen sensor detects the change.
- Volume flow of air is adapted for constant λ .
- But: volume flow of fuel remains constant !



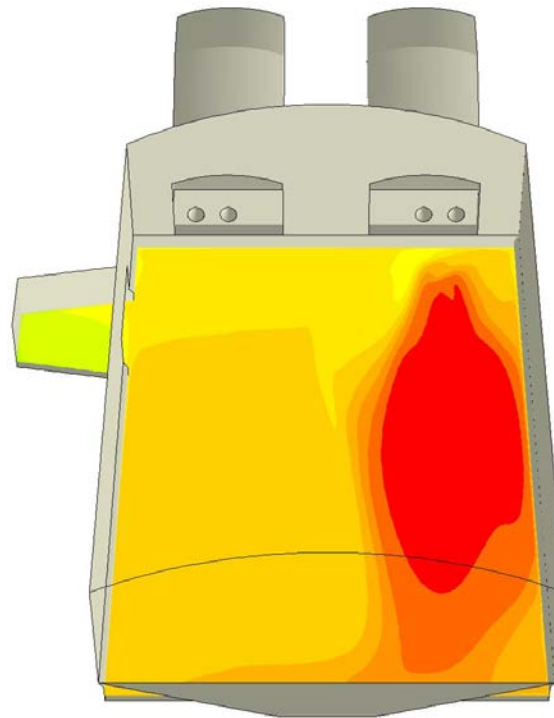
| Gas Type | $H_{i,n}$ [kWh/m ³] | Q_{Burner} [kW] | $\rho_{n,\text{Gas}}$ [kg/m ³] | $V_{n,\text{Gas}}$ [m ³ /h] | Air_{min} [m ³ _{Air} /m ³ _{Fuel}] | λ [-] | $V_{n,\text{Air}}$ [m ³ /h] |
|----------------|------------------------------------|-----------------------------|---|---|---|------------------|---|
| H-Gas Ref._GWI | 10.436 | 4000 | 0.8004 | 383.3 | 9.99 | 1.05 | 4021 |
| H-Gas 3_GWI | 11.884 | 4554 | 0.9043 | 383.3 | 11.27 | 1.05 | 4536 |
| H-Gas 1_GWI | 9.114 | 3494 | 0.7110 | 383.3 | 8.65 | 1.05 | 3482 |

Scenario I: Temperatures above the Glass Melt

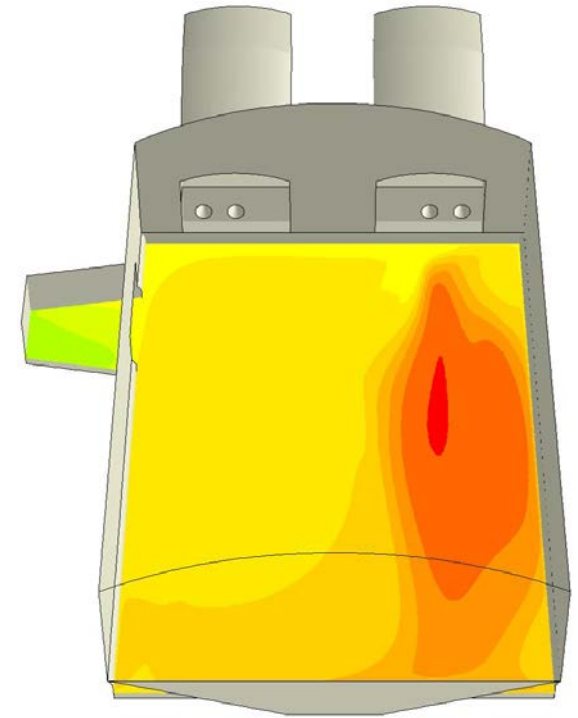
H-Gas Ref.-GWI



H-Gas 3_GWI

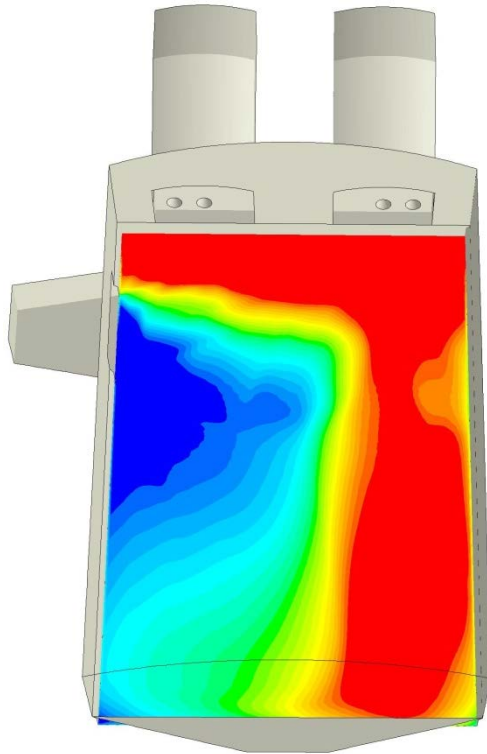


H-Gas 1_GWI



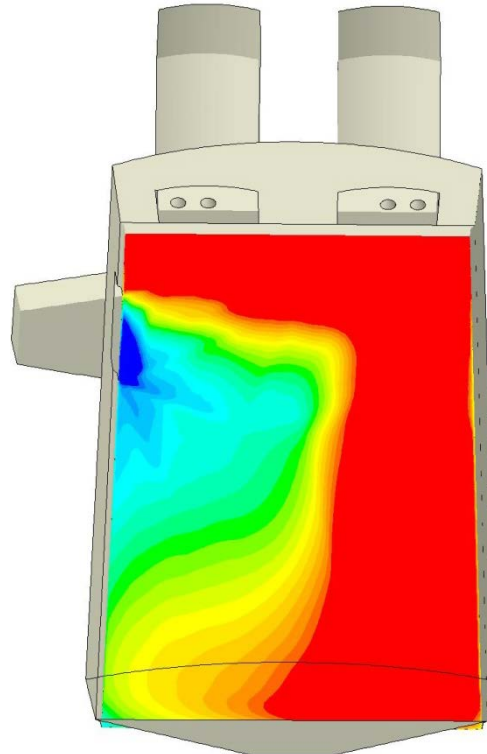
Scenario I: Total Heat Fluxes into the Glass Melt

H-Gas Ref._GWI



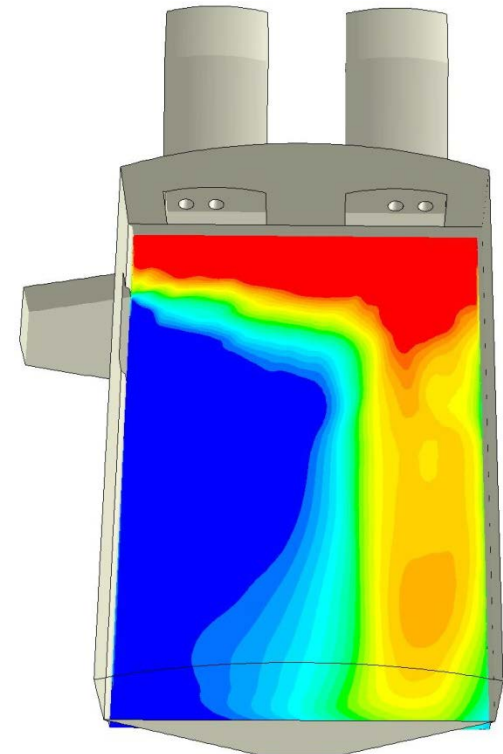
$Q = 1096 \text{ kW}$

H-Gas 3_GWI



$Q = 1455 \text{ kW}$
 $\Delta = 32.6 \%$

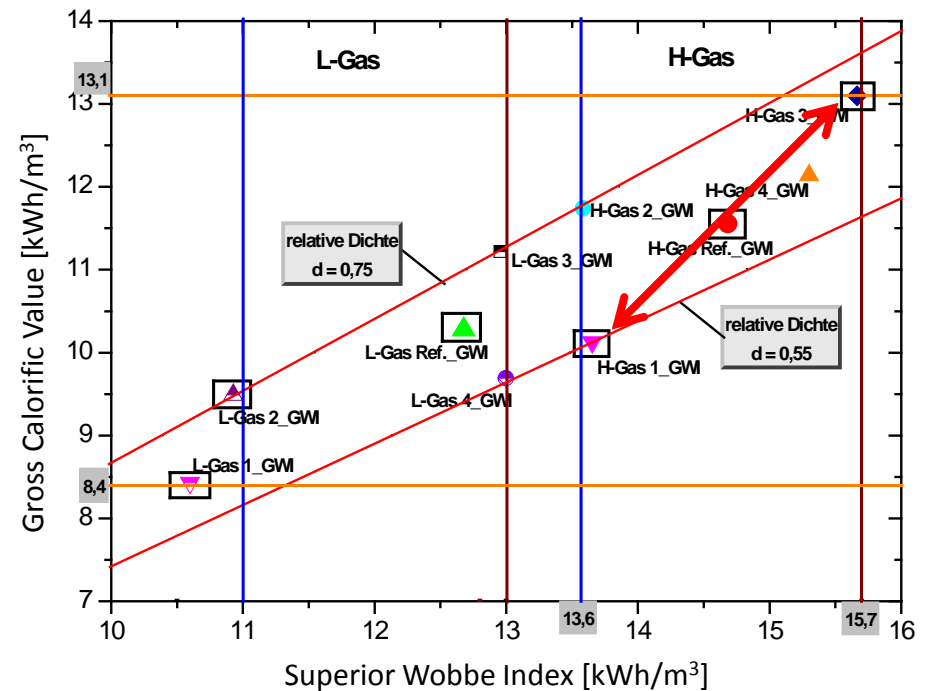
H-Gas 1_GWI



$Q = 741 \text{ kW}$
 $\Delta = -32.4 \%$



- Fuel gas composition changes from H-Gas Ref._GWI to H-Gas 1_GWI or H-Gas 3_GWI... and no one notices !
- Volume flows of **both** fuel and oxidizer remain constant.
- Definitely a worst case scenario !



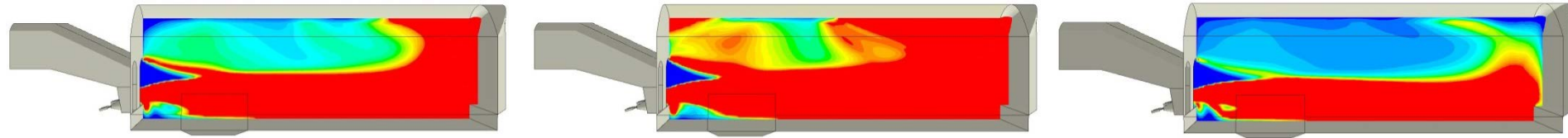
| Gas Type | $H_{i,n}$ [kWh/m³] | Q_{Burner} [kW] | $\rho_{n,\text{Gas}}$ [kg/m³] | $V_{n,\text{Gas}}$ [m³/h] | Air_{min} [m³ _{Air} /m³ _{Fuel}] | λ [-] | $V_{n,\text{Air}}$ [m³/h] |
|----------------|-----------------------|-----------------------------|----------------------------------|------------------------------|---|------------------|------------------------------|
| H-Gas Ref._GWI | 10.436 | 4000 | 0.8004 | 383.3 | 9.99 | 1.05 | 4021 |
| H-Gas 3_GWI | 11.884 | 4554 | 0.9043 | 383.3 | 11.27 | 0.93 | 4021 |
| H-Gas 1_GWI | 9.114 | 3494 | 0.7110 | 383.3 | 8.65 | 1.21 | 4021 |

Scenario II: Impact of Fuel Gas Changes

H-Gas Ref._GWI

H-Gas 3_GWI

H-Gas 1_GWI



| | | |
|---|--------|-------|
| Total Load | kW | 4000 |
| Air Ratio | - | 1.05 |
| CO₂ | Mole-% | 11.38 |
| N₂ | Mole-% | 87.39 |
| O₂ | Mole-% | 1.23 |
| H₂ | Mole-% | 0.00 |
| CO | ppm | 11 |
| NO_x @ 3 % O₂ | ppm | 3460 |

| | | |
|---|--------|-------|
| Total Load | kW | 4554 |
| Air Ratio | - | 0.93 |
| CO₂ | Mole-% | 11.11 |
| N₂ | Mole-% | 85.86 |
| O₂ | Mole-% | 0.00 |
| H₂ | Mole-% | 1.18 |
| CO | ppm | 18526 |
| NO_x @ 3 % O₂ | ppm | 1670 |

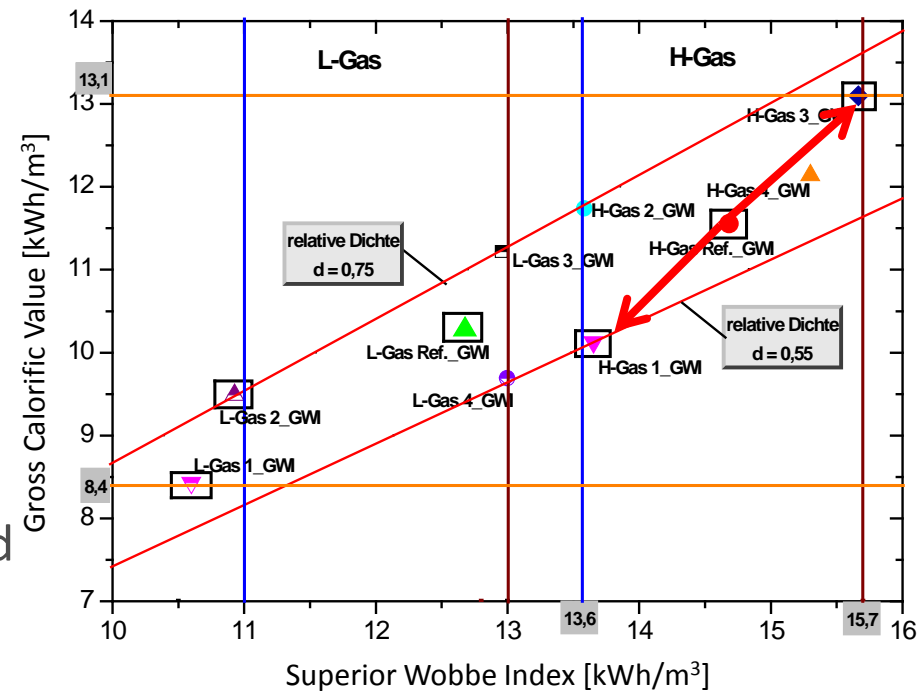
| | | |
|---|--------|-------|
| Total Load | kW | 3494 |
| Air Ratio | - | 1.21 |
| CO₂ | Mole-% | 9.50 |
| N₂ | Mole-% | 86.34 |
| O₂ | Mole-% | 4.16 |
| H₂ | Mole-% | 0.00 |
| CO | ppm | 3 |
| NO_x @ 3 % O₂ | ppm | 2850 |

0 200 400 600 800 1000 1200 1400 1600 1800 2000

CO_{dry} [ppm]



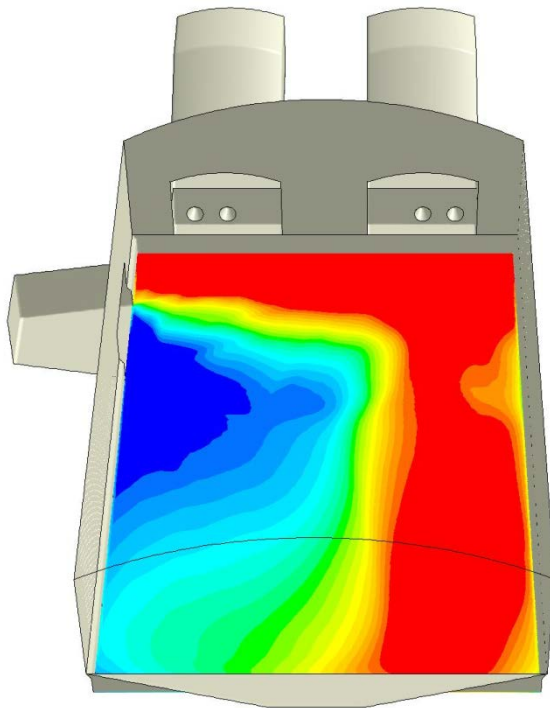
- Fuel gas composition changes from H-Gas Ref._GWI to H-Gas 1_GWI or H-Gas 3_GWI... fuel composition is constantly monitored (PGC).
- Volume flows of air and fuel are adapted for constant λ and burner load.
- Technologically, the most sophisticated solution... but expensive!



| Gas Type | $H_{i,n}$ [kWh/m³] | Q_{Burner} [kW] | $\rho_{n,\text{Gas}}$ [kg/m³] | $V_{n,\text{Gas}}$ [m³/h] | Air_{min} [m³ _{Air} /m³ _{Fuel}] | λ [-] | $V_{n,\text{Air}}$ [m³/h] |
|----------------|-----------------------|-----------------------------|----------------------------------|------------------------------|---|------------------|------------------------------|
| H-Gas Ref._GWI | 10.436 | 4000 | 0.8004 | 383.3 | 9.99 | 1.05 | 4021 |
| H-Gas 3_GWI | 11.884 | 4000 | 0.9043 | 336.6 | 11.27 | 1.05 | 4536 |
| H-Gas 1_GWI | 9.114 | 4000 | 0.7110 | 438.9 | 8.65 | 1.05 | 3482 |

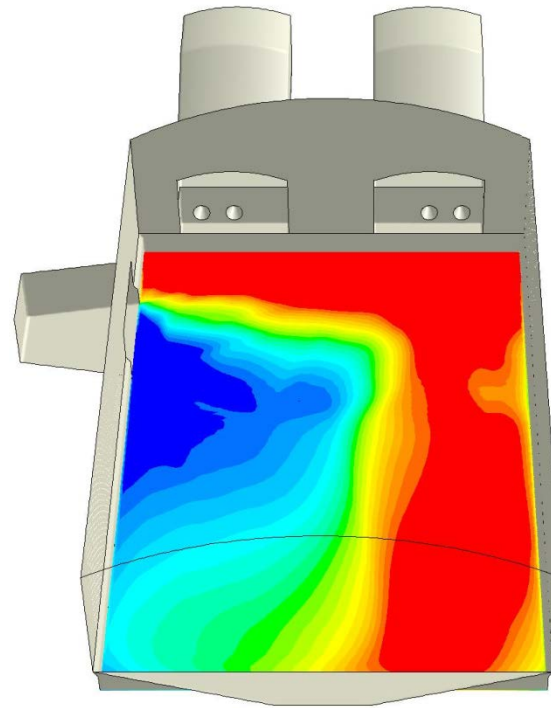
Scenario III: Total Heat Fluxes into the Glass Melt

H-Gas Ref._GWI



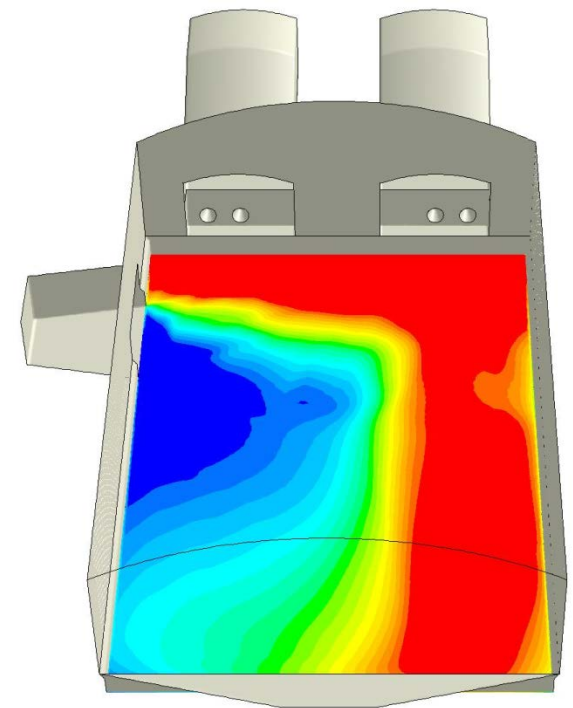
$Q = 1096 \text{ kW}$

H-Gas 3_GWI



$Q = 1102 \text{ kW}$
 $\Delta = 0.6 \%$

H-Gas 1_GWI



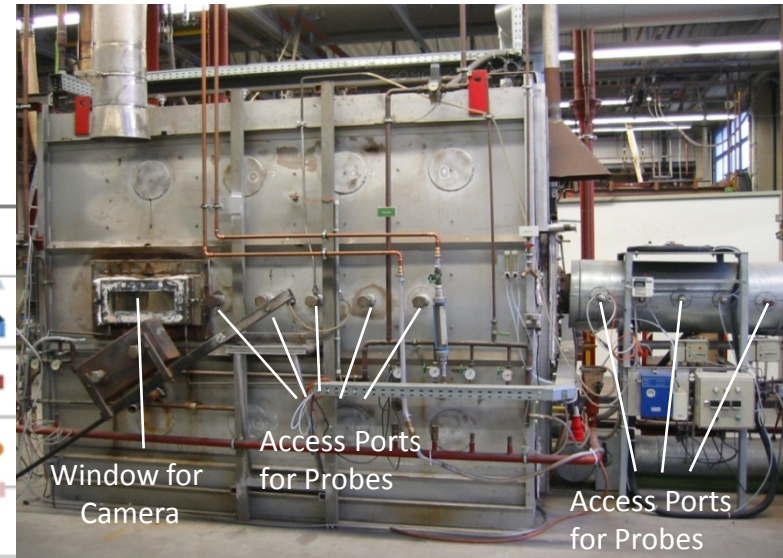
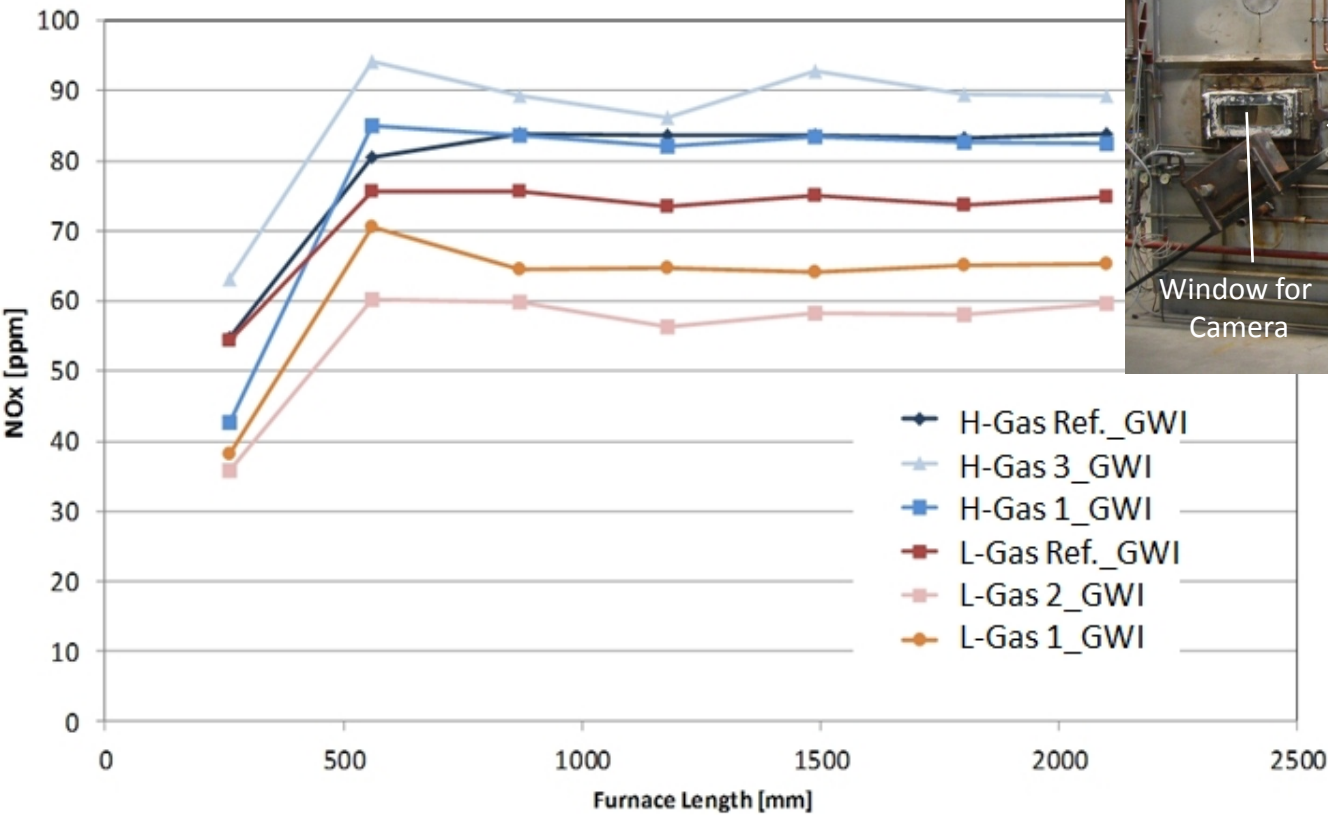
$Q = 1076 \text{ kW}$
 $\Delta = -1.8 \%$



Test Rig Measurements

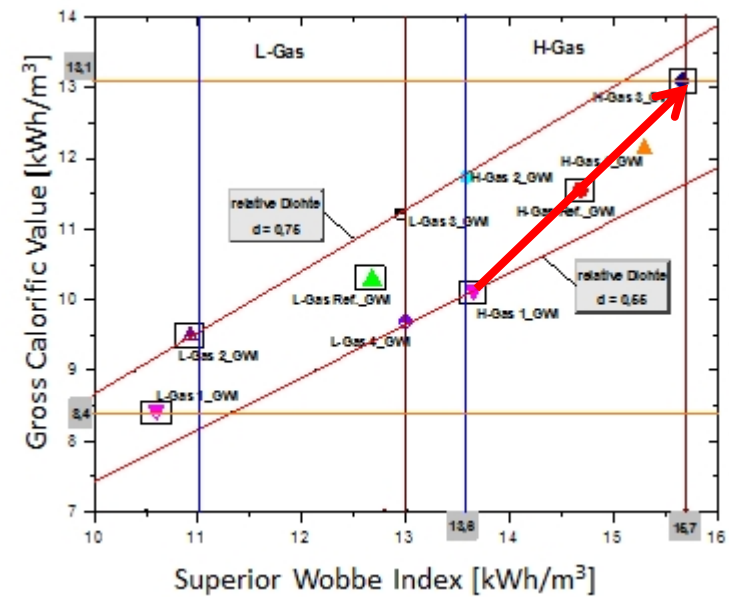
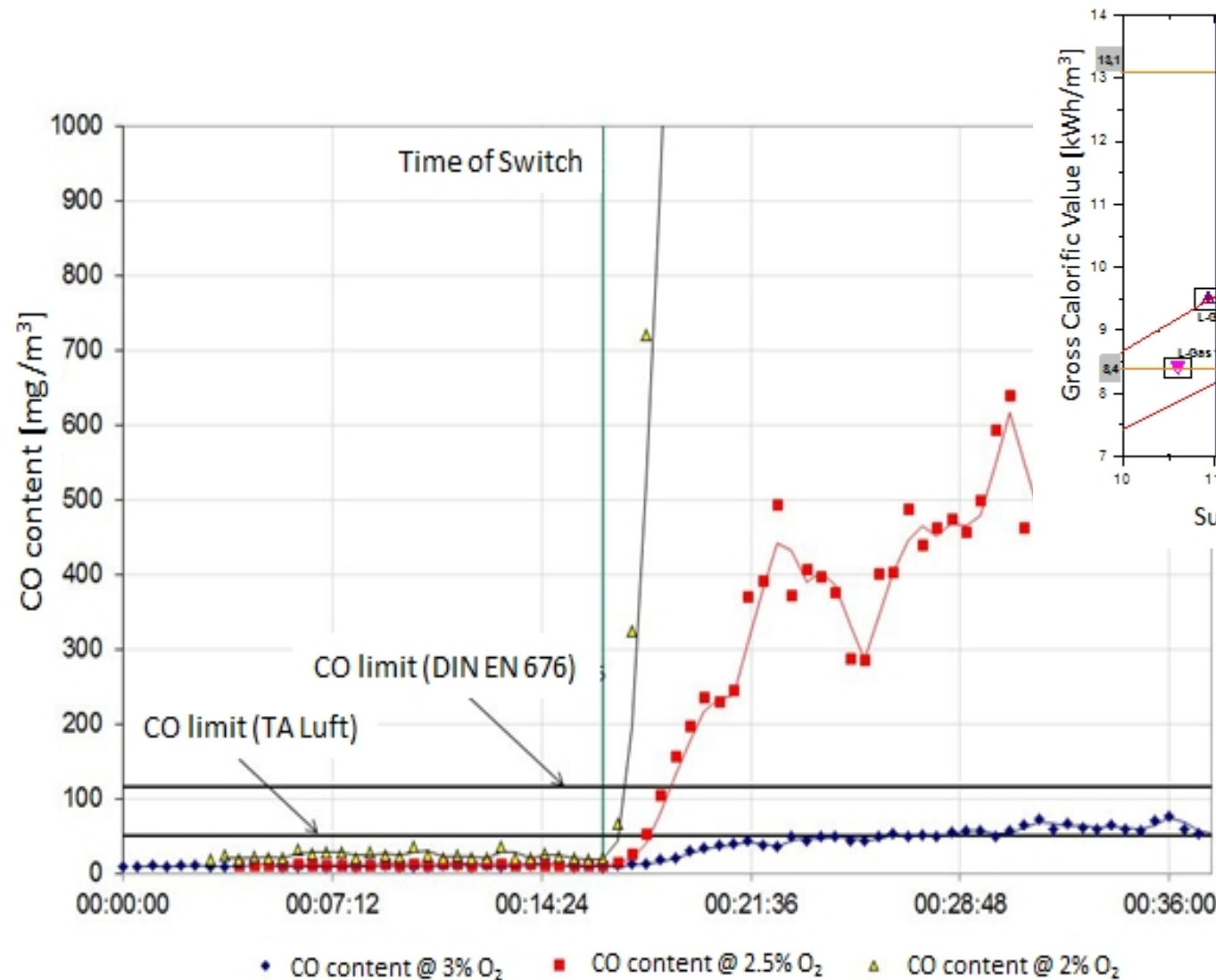


GWl Test Rig Measurements: NO_x along Central Axis






GWl Burner Test Rig: all measurements performed at $P = 200 \text{ kW}$, $\lambda = 1.15$, $T_{\text{air}} = 200 \text{ }^\circ\text{C}$

DBI Test Rig Measurements: Effect of Gas Switch on CO



| Industry | Process | Efficiency | Safety (Emissions and Thermal Overload) | Product Quality |
|--|-----------------------------------|------------|---|-----------------|
| When switching from lower to higher Wobbe Index (maximum possible range according to DVGW G 260) | | | | |
| Heat | boilers | Yellow | Red | Green |
| | luminous radiant heaters | Yellow | Red | Green |
| | direct and indirect drying | Yellow | Yellow | Yellow |
| Metallurgy | pre-heating (metals) | Yellow | Red | Yellow |
| | thermochem. heat treatment | Yellow | Yellow | Green |
| | zinc coating | Yellow | Green | Red |
| | melting (non-ferrous metals) | Red | Red | Red |
| Ceramics | calcination | Yellow | Yellow | Yellow |
| | brick & tiles manufacturing | Yellow | Red | Red |
| | porcelain firing | Yellow | Red | Red |
| Glass | glass melting (float) | Red | Red | Red |
| | glass melting (container), feeder | Red | Red | Red |
| | glass finishing treatment | Red | Red | Red |
| Other | chemical engineering, plastics | Red | Red | Red |

 no intervention required
 intervention possibly required
 intervention required

- The issue of fluctuating qualities of natural gas in the grids will play a bigger role for industrial gas consumers in the years to come. It is yet unclear how local gas quality changes will affect many industrial applications as they are typically not designed for such fluctuations.
- DVGW funded a research project to investigate and assess the susceptibility of various industrial gas-fired applications to gas quality changes. Some results were presented.
- There is no single way to prepare a thermal processing plant to fluctuating gas qualities. Every process is different and requires its own tailor-made solution.
- Advanced measurement and furnace control technologies can help mitigate the impact of fluctuating gas qualities. These may be significant investments especially for small and medium-sized enterprises.

DBI, EBI and GWI gratefully acknowledge the support by DVGW and our industrial partners in the supervisory committee.



The final report of the project (in German) is available at the GWI website:
www.gwi-essen.de



Thank you for your attention !

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