

the Energy to Lead

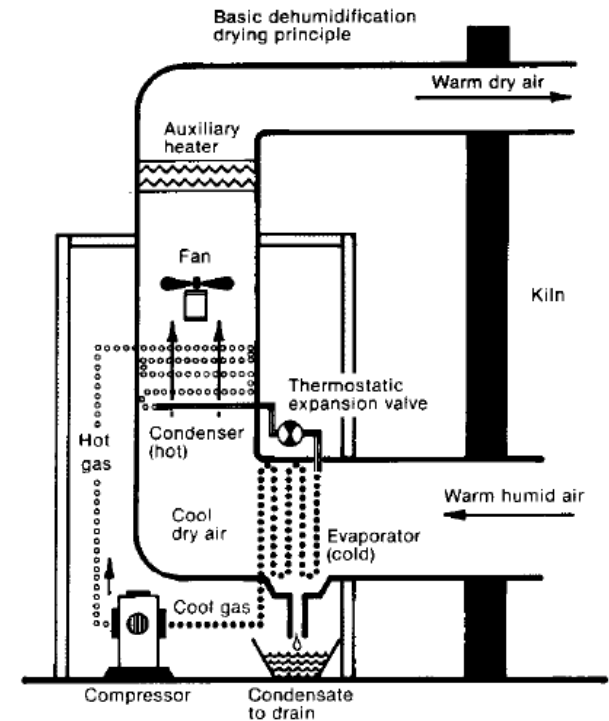
Industrial Heat Pumps in Agricultural Drying Applications

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U.S. AGRICULTURAL DRYING

Opportunity for Thermal-Driven Heat Pumps

- > Indirect drying is a significant natural gas load in North America, 5% of the U.S. Commercial and Industrial gas consumption.
- > Drying step can consume between 50-70% of process energy to deliver finished product in agricultural and lumber applications.
- > The same overall design has been in use for over 50 years, with a nominal efficiency of 35%, with advanced technologies reaching 82%-88%.
- > The industry has explored vapor compression (VC) heat pump drying (HPD) since 1973, though market impact since has been limited – due to high relative cost of electricity at **6.5X that of natural gas** (US DOE – 2012).
- > Thermally-driven HPD makes good sense, simultaneous heating and dehumidification with a lower temperature lift than other heat pump applications.



USDA Agricultural Handbook AH-188: *Dry Kiln Operator's Manual* (2001)
http://www.fpl.fs.fed.us/products/publications/several_pubs.php?grouping_id=101&header_id=p

U.S. AGRICULTURAL DRYING

Opportunity for Thermal-Driven Heat Pumps

- > To evaluate this opportunity, GTI is leading a team to develop and demonstrate a hybrid Gas-Fired Rotary Dryer with Integrated Heat Pump for Ag drying in California.
 - Drying fruits and vegetables in CA requires 1,815 GWh/year
- > Team includes:
 - Manufacturers of Drum Dryer (GL&V) and Burners (Flynn)
 - HPD Technology Developer for Ejector Heat Pump (May-Ruben Thermal Solutions)
 - Food processor host site (Bean Drying)
 - CA Utility Partners

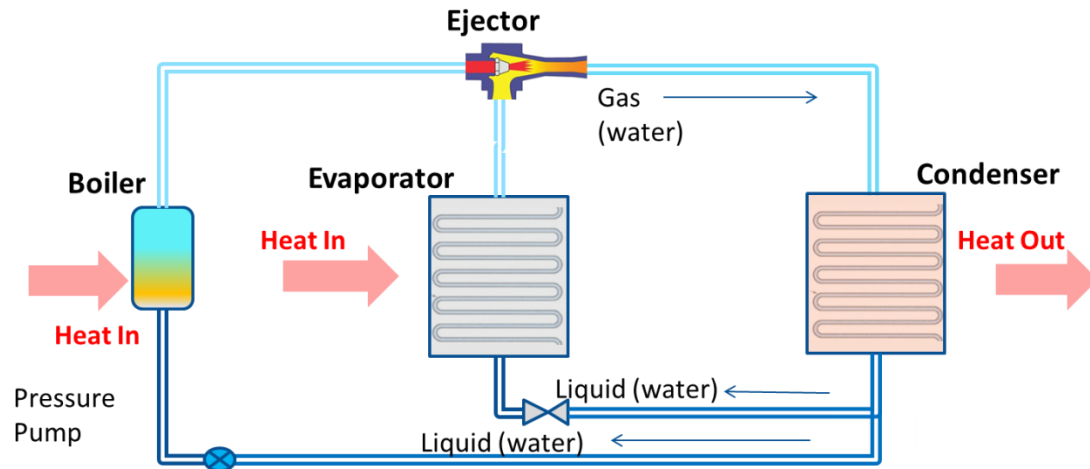
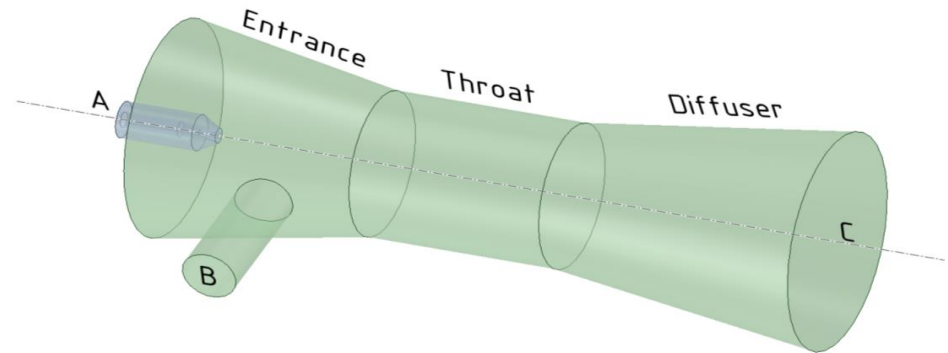


GTI Drum dryer demonstration in paper drying facility

EJECTOR HPD SYSTEM CONCEPT

Ejector Heat Pumps, Then...

- > As a 'thermo-compressor', ejectors can compress a low pressure gas or saturated vapor with a high pressure fluid.
- > Simple system for compression when steam or waste heat is available, standard ejectors were used for refrigeration & ice production since 19th Century.
- > Standard systems had $COP_{cooling} < 0.3$, small entrainment ratios, not common today



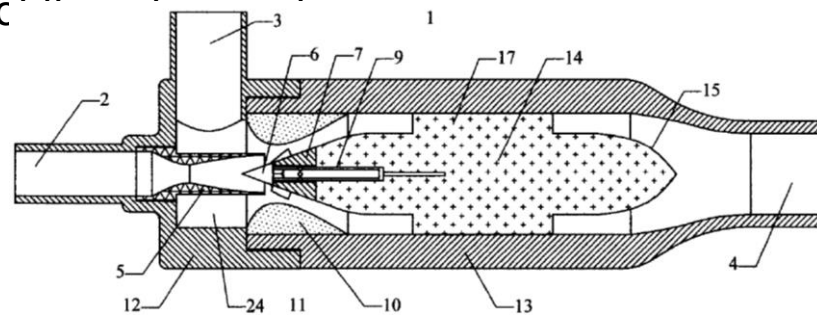
EJECTOR HPD SYSTEM CONCEPT

Ejector Heat Pumps, Then...

Two major problems limit ejector performance:

- > Single working fluid needed for two distinct jobs, compromises by doing both poorly.
 - > **Refrigeration** – Fluid must have a high enthalpy of vaporization for near isothermal phase change in condenser/evaporator. Heat transfer efficiency & capacity drop when non-isothermal.
 - > **Ejector Entrainment**– Fluid must **not** have a high enthalpy of vaporization to boil easily in the generator, improving COP. Also, entrainment is aided when the molecular mass of the drive fluid exceeds that of the refrigerant.

- > Principle method of compressing refrigerant during entrainment is *momentum exchange*, inefficient turbulent mixing. *Pressure exchange* is much better, with the drive fluid providing “mechanical” compression.



Garris, C. A., GWU “Pressure Exchanging Ejector and Methods of Use”.
U.S. Patent 6,138,456.

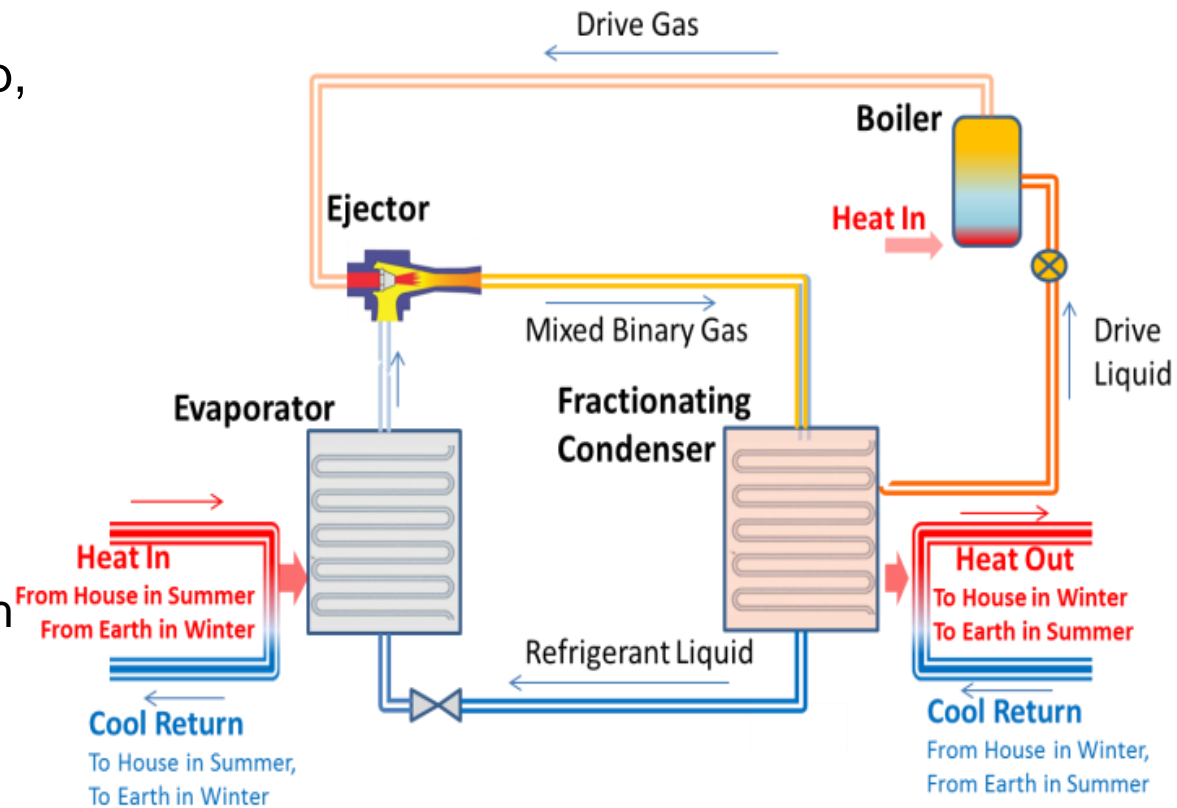
EJECTOR HPD SYSTEM CONCEPT

Ejector Heat Pumps, Now

> May-Ruben Thermal Solutions has developed the Binary Fluid Ejector (BFE) heat pump, for non-incremental improvement over standard ejectors:

> **Two fluids, engineered for respective roles**

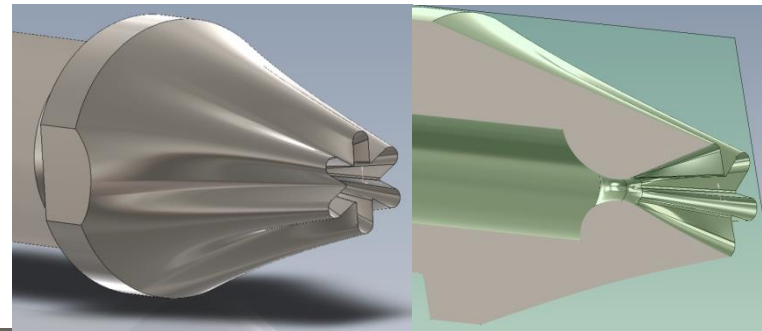
> Novel nozzle designs to promote pressure energy exchange, static designs with vortex columns or, in later possible developments, dynamic with oscillating nozzle



EJECTOR HPD SYSTEM CONCEPT

Ejector Heat Pumps, Now

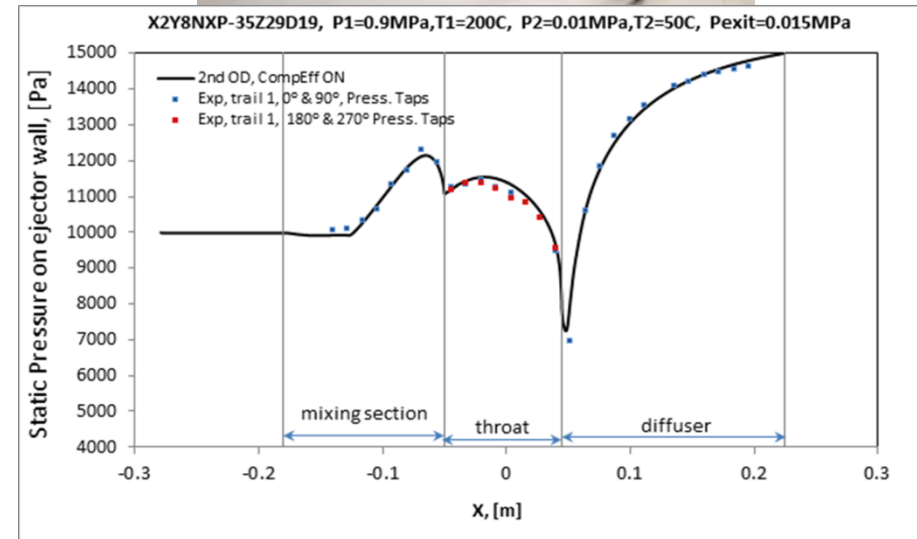
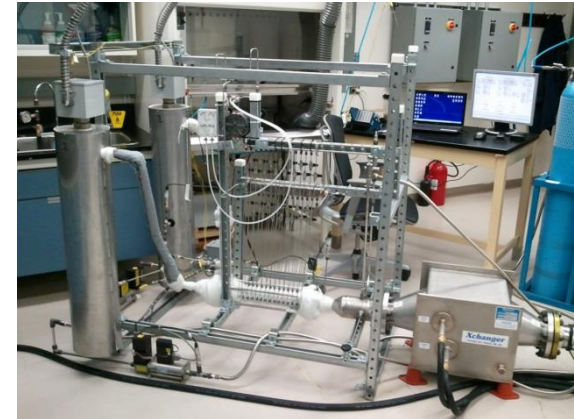
- > May-Ruben Thermal Solutions has developed the Binary Fluid Ejector (BFE) heat pump, for non-incremental improvement over standard ejectors:
 - > Two fluids, engineered for respective roles
 - > **Novel nozzle designs to promote pressure energy exchange, static designs with vortex columns or, in later possible developments, dynamic with oscillating nozzle**



EJECTOR HPD SYSTEM CONCEPT

Ejector Heat Pumps, Now

- > Initially focusing on desalination, extensive combination of parametric analysis with experimentally-validated CFD simulation and testing with inert gases in ejector test rig completed:
 - > Entrainment ratios and estimated COPs, when extrapolated to seasonal temp. lifts show exceeding heating/cooling COPs of 2.0/0.9 may be feasible.
 - > Depending on ultimate fluid pair selection, operating pressures may be quite moderate ($\ll 100$ psi/0.7 MPa).
 - > With quick startup, ejectors may be deployed in parallel for modulation



Example of CFD model calibration with inert gas

EJECTOR HPD SYSTEM CONCEPT

Ejector Heat Pumps, Now

> Simplified analysis shows critical impact of binary fluid selection and ejector design, guides optimization process and performance estimates:

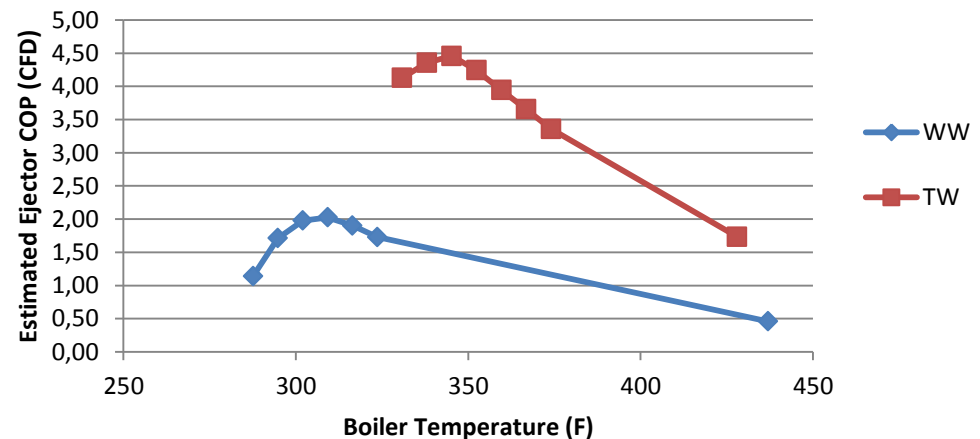
> Entrainment ratio (m_R/m_D) is largely a function of the nozzle design and ratio of fluid MW

> f_h is a function of fluid selection and operating conditions

$$COP = \frac{Q_{evaporator}}{Q_{boiler} + W_{pump}} = \omega \frac{(h_{s,out} - h_{s,in})_{evap}}{(h_{p,out} - h_{p,in})_{boiler} + \frac{(P_{p,out} - P_{p,in})_{pump}}{\rho_{avg, in\ out}}}$$



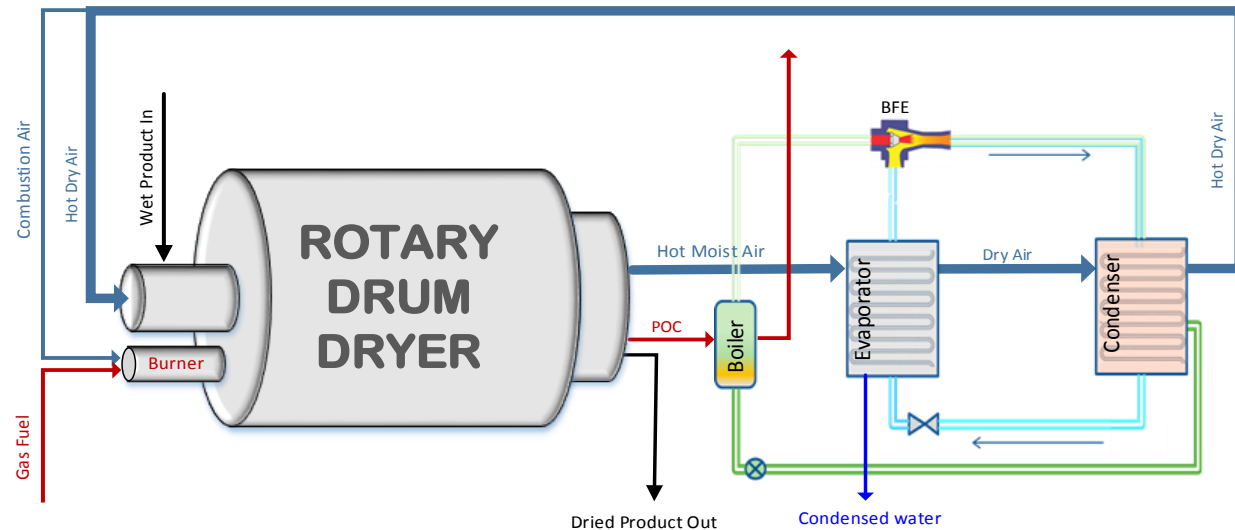
$$COP = \omega \frac{Hv_{Evap} + \overline{Cp}_1(T_{Cond} - T_{Evap})}{Hv_{Boil} + \overline{Cp}_2(T_{Boil} - T_{Cond})} = \omega f_h$$



GAS-FIRED HPD IN CALIFORNIA

Next Steps in the Development

- > While early-stage development, with remaining technical risks, opportunity is large:
 - Energy savings versus standard gas drying.
 - Capital and operating cost savings versus existing HPD options.
- > RD&D program initiating now.



Heat Source	Output Energy (MWh)	COP	Input Energy Required (MWh)	Annual** Energy Cost (\$)	% Cost Savings vs gas heat	Annual Cost Savings (\$) vs gas heat
Direct Fired Gas	1	0.8	1.25	\$ 233,235	-	-
Electric HP	1	4.0	0.25	\$ 197,100	15%	\$ 36,135
BFE HP	1	2.0	0.50	\$ 93,294	60%	\$ 139,941

**based on natural gas rate \$0.22/m³ and electrical rate of \$0.09/kWhr at annual operations of 350 days/year

Connect With Us

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